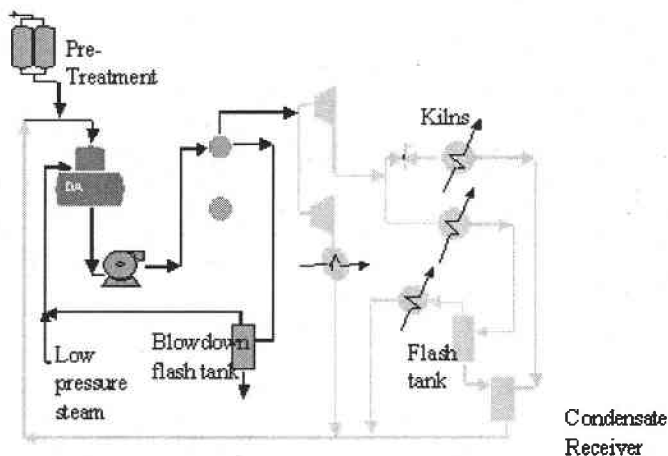


# THE CONDENSATE STORY

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## Overview

- The value of condensate
- Condensate corrosion
- System survey
- Condensate treatment
  - mechanical
  - chemical
- Monitoring and control



## The Value of Condensate

### Heat:

Reduced fuel usage - typically \$6-13 per 1000 gal

### Water:

Decreased makeup water demand  
Decreased pretreatment costs  
Reduced water discharge

### Boiler Reliability

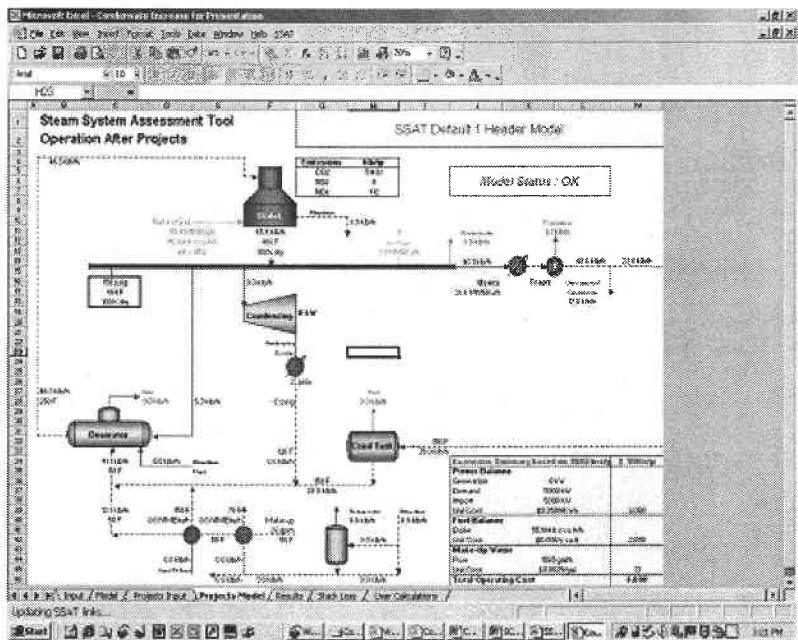
Improved feedwater quality

Calculate the Value of Condensate

Potential Savings =  $\frac{H_f \times C}{FV \times B} \times FC$

- Where:
- $H_f$  = difference in hf between condensate stream and make-up (Btu/hr)
  - $C$  = condensate stream flow (lbs/hr)
  - $FV$  = heat value of fuel (Btu/fuel unit)
  - $B$  = boiler efficiency (%)
  - $FC$  = cost of fuel (\$/fuel unit)

Use of Steam System Assessment Tool



Microsoft Excel - Condensate Increase for Presentation

File Edit View Insert Format Tools Data Window Help 2004

100%

Sheet1

A B C D E F G H

### Steam System Assessment Tool

#### 1 Header Model

#### Results Summary

#### SSAT Default 1 Header Model

Model Status: OK

Cost Summary (\$/MWh/yr)	Current Operation	After Projects	Reduction
Power Cost	2,000	2,000	0 0.0%
Fuel Cost	2,661	2,659	29 0.6%
Maintenance Water Cost	41	31	10 23.5%
<b>Total Cost (\$/MWh/yr)</b>	<b>4,722</b>	<b>4,690</b>	<b>32 0.7%</b>

**10% CR Increase = \$32,000 / year fuel savings**

On-Site Emissions	Current Operation	After Projects	Reduction
CO <sub>2</sub> Emissions	5193 kbt/yr	5193 kbt/yr	0 0.0%
SO <sub>x</sub> Emissions	0 kbt/yr	0 kbt/yr	0 0.0%
NO <sub>x</sub> Emissions	100 kbt/yr	100 kbt/yr	0 0.0%

Power Station Emissions	Current Operation	After Projects	Total Reduction
CO <sub>2</sub> Emissions	5193 kbt/yr	5193 kbt/yr	0 0.0%
SO <sub>x</sub> Emissions	0 kbt/yr	0 kbt/yr	0 0.0%
NO <sub>x</sub> Emissions	100 kbt/yr	100 kbt/yr	0 0.0%

Note: Calculates the impact of the change in site power input on emissions from an external power station. Total reduction values are for site + power station.

Utility Balance	Current Operation	After Projects	Reduction
Power Generation	0 kW	0 kW	0 0.0%
Power Input	5000 kW	5000 kW	0 0.0%
Total Site Electrical Demand	5000 kW	5000 kW	0 0.0%
Boiler Duty	55.9 MMStk/h	55.4 MMStk/h	0.5 MMStk/h 0.9%
Fuel Type	Natural Gas	Natural Gas	

Model: 1 Header Model / Project: Input / Results / Stack: OK / User: Calculations /

Results Calculate

2:32 PM

## Results of Condensate Corrosion

- Frequent kiln coil replacement
- Steam/condensate line replacement
- Excess iron entering boiler
  - efficiency loss
  - deposits result in potential tube ruptures
  - boiler cleaning due to iron deposits
- Unscheduled outages

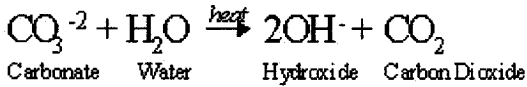
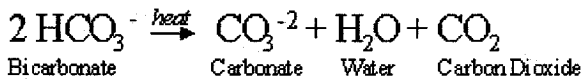
## Primary Causes of Condensate Corrosion

Condensate treatment is the battle against three dissolved gases:

carbon dioxide	(CO <sub>2</sub> )
oxygen	(O <sub>2</sub> )
ammonia	(NH <sub>3</sub> )

## Carbon Dioxide Comes from Alkalinity in Make-Up Water

Breakdown of feedwater alkalinity

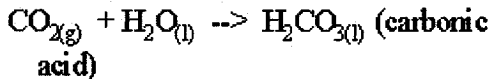
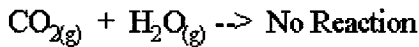


Air in leakage

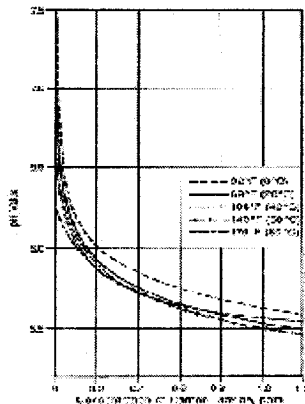
Pumps, receivers, etc.

## Carbon Dioxide

Dissolves in the condensate forming carbonic acid

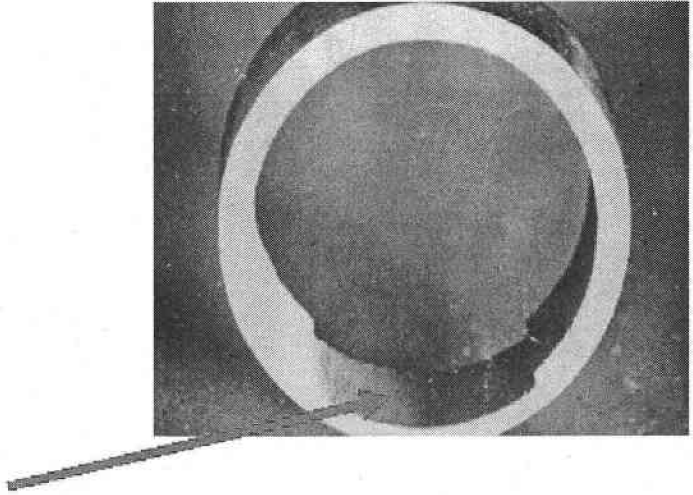


## pH Value of CO<sub>2</sub> in Pure Water at Various Concentrations



## Carbonic Acid Corrosion

Results in a thinning and grooving of the metal surface. Usually on the pipe where the condensate lays.

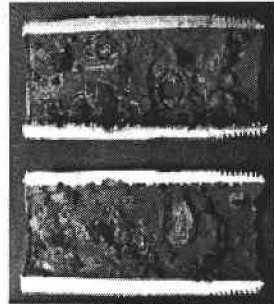


## Oxygen Sources

- Air in-leakage: pumps, traps, vacuum systems, vented receivers, week-end shutdowns
- Inefficient deaeration operation
- Raw water intrusion: pump seals, heat exchanger leaks

## Oxygen Corrosion

- $O_2$  attack results in pitting type corrosion.
- Rapid localized metal loss.
- Combined corrosion rate of carbon dioxide and oxygen is 10-40% faster than the sum of either alone.



## **System Survey**

- A complete system survey is the key to any effective corrosion prevention strategy.
- The survey defines system needs and limitations allow for proper MOC solution
  - Mechanical
  - Operational
  - Chemical

## **Key Considerations**

- Make-up water quality
  - CO<sub>2</sub> generation
- Percent condensate return
  - amine recycled, determines makeup quantity
- Potential for system contamination
- System configuration and complexity (steam uses)
  - amine selection

## **Mechanical Reduction of Corrosion Potential**

- Prevent stagnation/coil water logging
- Reduce air in leakage
- Assure proper deaeration
- Reduce feedwater alkalinity

## **Mechanical: Steam Trap Maintenance**

- Annual maintenance checks
- Four-six years, 50 percent of traps will likely be failing open or closed
- Efficiency/corrosion
- Problems do not surface until too late w/o a formal trap program

## **Mechanical: Condensate Delivery Potential Issues**

- Above ground condensate recovery tanks
  - rely on steam pressure through coils to elevate to the height of tank
- Condensate pumps not utilized
  - rely solely on steam pressure to push condensate to boiler house
- Both can result in stagnant condensate
  - elevated corrosion rates
  - decreased coil efficiency

## **Operational/Mechanical Common Air In-Leakage Sites**

- Vacuum systems
- Vented receivers
- Condensate pumps, traps, and valves
- Intermittently operating systems

## **Operational: Feedwater Alkalinity Reduction**

- Lime softening
- Reverse osmosis

- Dealkalization
- Demineralization
- Increased condensate return

### Chemical: Condensate Treatment

- Neutralizing amines
- Filming amines

### Condensate Treatment Requirements

- Effective corrosion protection
- Distribution throughout system
- Which chemistry do we primarily use to combat carbonic acid?

### Why Amines are so Popular

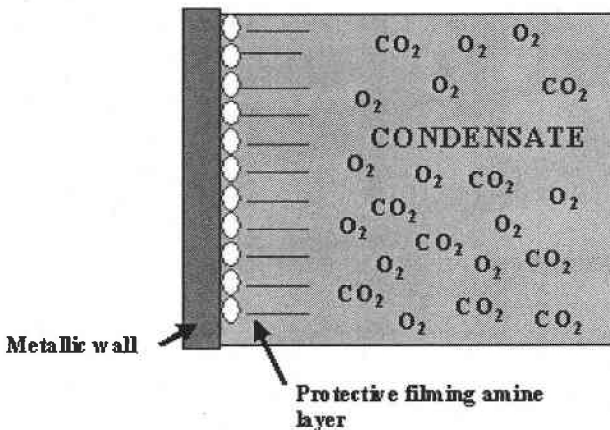
- Direct neutralization of  $\text{CO}_2$
- Direct elevation of pH
- Easy to feed/control
- Compatible with other system treatments
- Treatment recycles
- Blends available: able to distribute through entire systems

### Neutralizing Amines Limitations/Considerations

- Not effective against oxygen
- Perhaps not best choice in high alkalinity waters
- Not all locations will have same pH: a blend of amines is typically required  
good distribution  
volatility ratio

### Filming Amines

- Long chain amines that absorb onto the metal surface
- Function at the lower pH range of 6.5 to 9.0



- Protect against acids, O<sub>2</sub>, and ammonia
- Dosage dependent on surface area and not contaminant concentration
- Cost effective in high CO<sub>2</sub> systems

### **Filming Amines Limitations/Considerations**

- Film formation takes time
- pH control still necessary
- Should be fed after turbines and condensate polishers
- Will clean up old deposits
- Overfeed may cause sticky deposits and "gunk" ball formation
- Nalco ACT

### **Quality Control: Condensate Monitoring**

- pH
- Conductivity
- Corrosion rates
- Corrosion byproducts

### **Secondary Testing and Troubleshooting**

- Dissolved oxygen
- Hardness
- Silica
- Ammonia
- Alkalinity
- Product residual

### **Corrosion and Corrosion Byproducts**

- Grab samples
  - filtration millipore testing
  - wet chemistry
    - colorimeter testing
      - \* total iron
      - \* insoluble iron (particulate)
      - \* soluble iron (indicative of recently corrosion activity)
- Corrosion coupons
- Corrosion sensor

### **Nalco Corrosion Sensor**

- Monitors corrosivity of condensate
  - real time indication
- Provides direct MPY readings up to 300°F
- Collects and displays all data

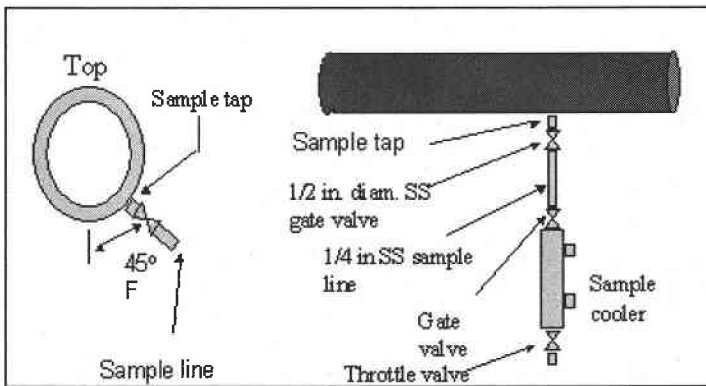
## Sampling Requirements

- Cooled to less than 90 °F\* (pH)
- Sample flow throttled at outlet only\*
- Stainless steel sample lines
- Continuous flow
- Adequate velocity

## Sampling

- Sample tap locations
- 45 degrees off bottom of horizontal pipe
- Representative of system
- Prior to condensate receivers\*

## Sampling Horizontal Lines



## Key Take-Aways

- Condensate is a precious commodity  
Never underscore its value  
Take every opportunity to return as much condensate as possible, look for lost condensate, it is out there.
- Every system is unique  
Complete proper survey
- Always mechanical before chemical  
Alkalinity removal prior to boiler  
Check each trap once per year  
Proper flow for condensate return
- Proper condensate monitoring in place